

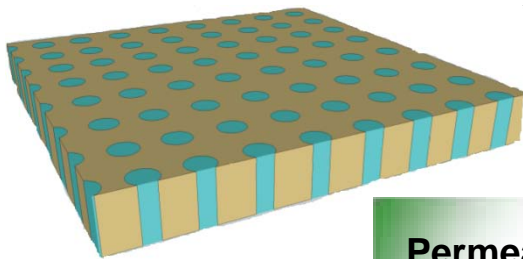
Gelled Ionic Liquid-Based Membranes

Rajinder P. Singh, Kathryn A. Berchtold, Richard D. Noble,
Douglas L. Gin, Abhoyjit Bhowm and Laura Nereng

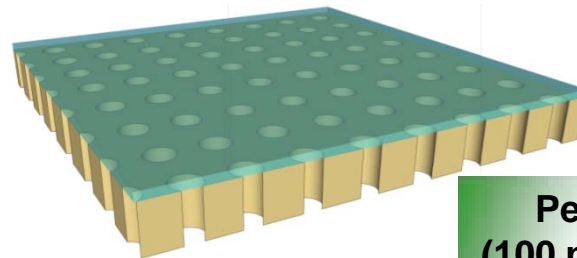
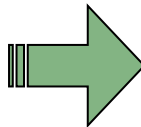
2013 NETL Carbon Capture Technology Meeting
Pittsburgh, 11th July, 2013

Project Objectives and Goals

- A carbon-capture membrane with **CO₂ permeance** approaching **5,000 GPU** and moderate CO₂/N₂ selectivity could significantly reduce cost of post-combustion carbon capture from flue gas
- Room-temperature ionic liquids (**RTILs**) are attractive materials due to **high permeability (>1000 barrer)** and good **CO₂/N₂ permselectivity (20–50)**
- To meet performance target, RTILs must be ***immobilized as a continuous, defect-free thin film, ca. 100 nm thick*** (permeability dependent), on a porous support - achievable via industrially relevant coating/fabrication techniques



Permeability = 500 barrer



Permeance (100 nm thick SL) = 5,000 GPU

Project Overview

- **Project Start Date: Feb. 1, 2011**
- **End Date: Jan. 31, 2014**
- **Total funding: \$3,927,591**
 - **DOE ARPA-E: \$3,142,071**
 - **DOE cost share numbers: \$785,520 (of which \$600,000 is provided by TOTAL, S.A.)**
- **This work is a result of a collaboration between the**
 - University of Colorado (CU), Boulder**
 - Los Alamos National Laboratory (LANL)**
 - Electric Power Research Institute (EPRI)**
 - 3M**
 - TOTAL, S.A.**

Project Team



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Key Milestones

BP01	<p>Title: Assessment of Ability of Proposed Technology to Meet Project Permeance & Selectivity Targets</p> <p>Criteria:</p> <ul style="list-style-type: none"> • Demonstration of ability to increase permeance by \geq an factor of 2 over benchmark data using material modifications and membrane fabrication optimization • Demonstrate membrane CO_2/N_2selectivity ≥ 20 • Demonstrate membrane adhesion at predicted process temperatures ($>50^\circ\text{C}$) 	Completed
BP02	Down-select and rank selective layer materials with highest potential to achieve project goals and DOE Program targets	Completed
BP02	Down-select and rank selective layer materials and material/coating methodology combinations with highest potential to achieve project goals and DOE Program targets	Completed
BP02	Report results of preliminary membrane process design based on initial membrane performance data	In-progress
BP03	<p>Title: Assessment of Ability of Proposed Technology to Meet ARPA-E, DOE-FE NETL Program Targets (cost and carbon emissions reduction) as Defined via Systems & Economic Analysis</p> <p>Criteria: Demonstration of ability to meet project's permeance and selectivity targets (5000 GPU, CO_2/N_2selectivity ≥ 20).</p>	In-progress

Project Tasks

- **Selective Layer Design Synthesis & Evaluation**
 - Tailored gel-RTILs, RTIL/poly(RTIL) composites, incorporation of task-specific CO₂ complexation chemistries
 - Optimize *permeability/selectivity* and *material properties* of Selective Layer Materials
- **Ultra-Thin Membrane Fabrication, Optimization, & Testing**
 - Commercially viable fabrication techniques development for new RTIL-based materials - to enable controlled ultra-thin SL deposition on commercially attractive support platforms
 - Ultrasonic spray coating technique (USCT)
 - Roll to roll casting
- **Membrane, Systems, and Economic Analyses**

Project Overview


 University of Colorado **Boulder**




**Selective Layer
Material Design and
Synthesis**

**Ultra-Thin Membrane
Fabrication**

**CO₂ Permeance
≥ 5,000 GPU**
**CO₂/N₂ selectivity
≥ 20**

**Systems Process
Modeling**


 ELECTRIC POWER
RESEARCH INSTITUTE

Membrane Terminology

➤ **Permeability** is a *material* property: describes rate of permeation of a solute through a material, normalized by its thickness and the pressure driving force

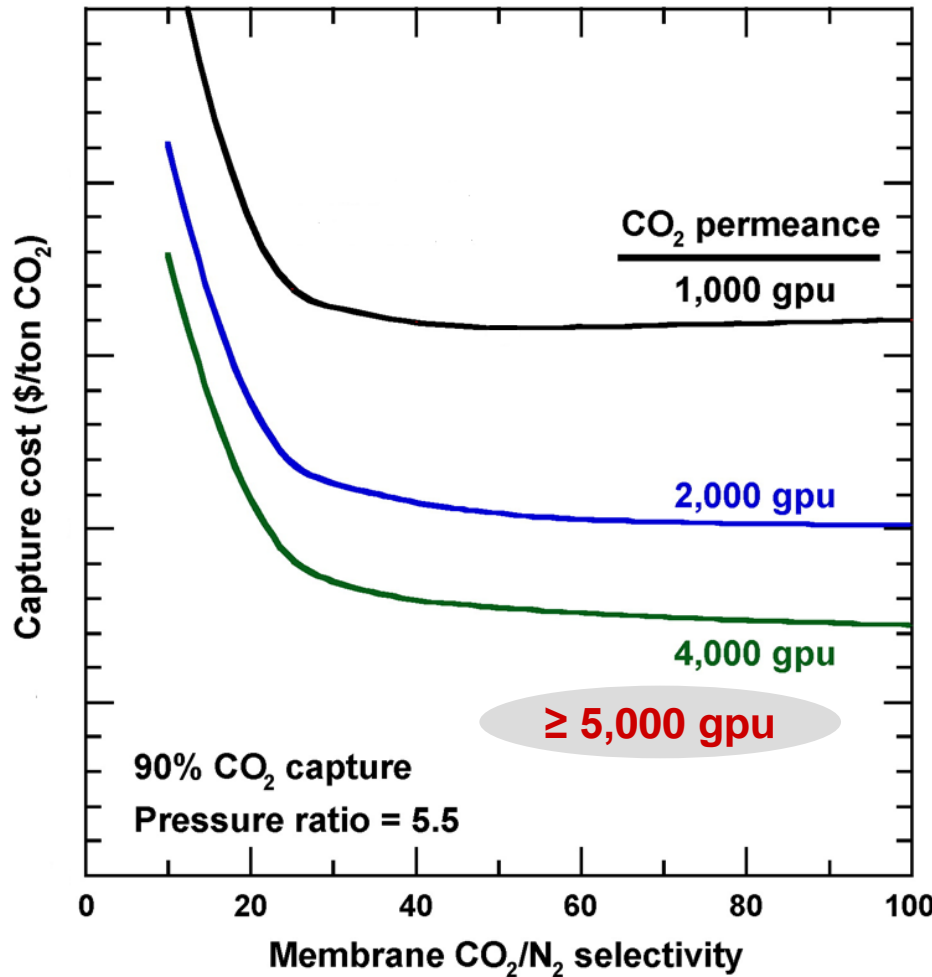
$$\text{Permeance} = \frac{\text{Permeability}}{\text{Thickness}} = \frac{\text{Flux}}{\Delta p}$$

➤ **Permeance** is a *membrane* property: calculated as solute flux through the membrane normalized by the pressure driving force (but not thickness)

➤ **Ideal selectivity** describes separation factor: the ratio of permeability (or permeance) of two different components in a membrane, and is a *material* property

➤ High membrane **permeance** is achieved by both material selection (high **permeability**) and membrane design (low **thickness**)

High Permeance – Economic Advantages



- Membrane separation systems with high CO₂ permeance and moderate CO₂/N₂ selectivity are desirable
- Estimated capture cost is proportional to CO₂ permeance for CO₂/N₂ selectivities greater than 30

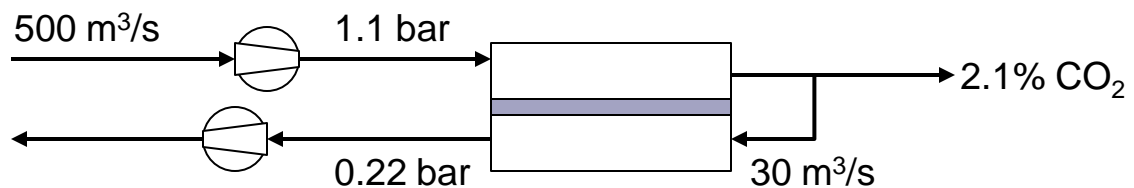
“Higher CO₂ permeance will lead to reduction in capture cost”

Adapted from: T. C. Merkel et al., *J. Memb. Sci.*, 359, 2010, 126-139.

Preliminary Economic Evaluation

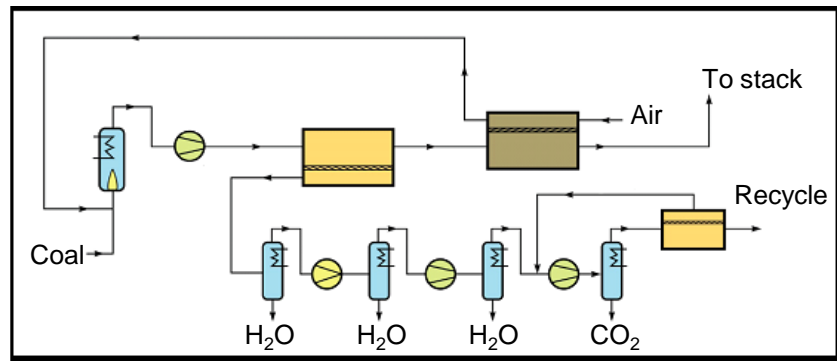
➤ Task 1: Benchmarking with MTR results

Single counter current sweep stage



Case	Membrane area (MM m ²)	Total power MTR* (MW)	Total power This work (MW)
Dry feed	4.3	46.4	44.6
Wet feed	3.9	47.2	53.1

The MTR process

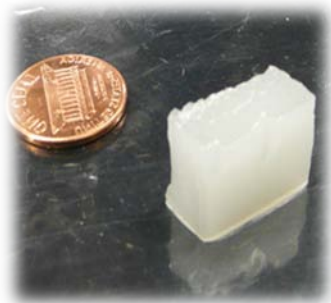


Total Area 1.3 MM m² **Blower pressure** 2 bar
Capture Rate 90% **Vacuum pressure** 0.2 bar

Total power required (MW)	
MTR	This work
97	102

Bulk RTIL Membrane Materials Overview

Gelled RTIL



Linear Poly(RTIL)/RTIL Composites

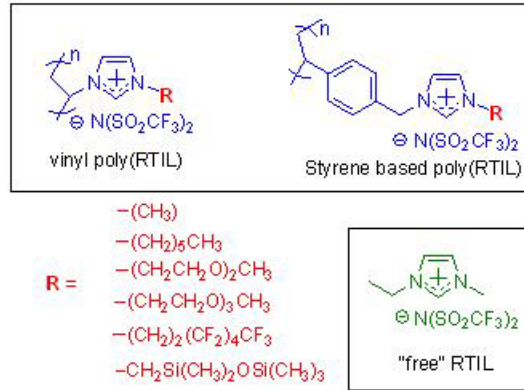
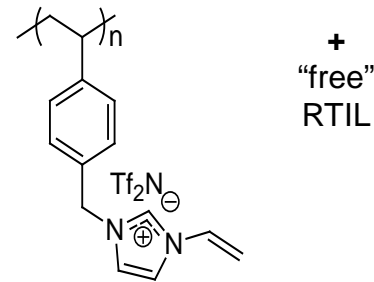
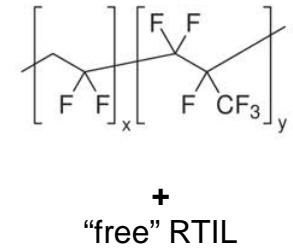


Photo-curable Poly(RTIL)s and Composites



PVDF-co-HFP/RTIL Composites



Evolution of Materials

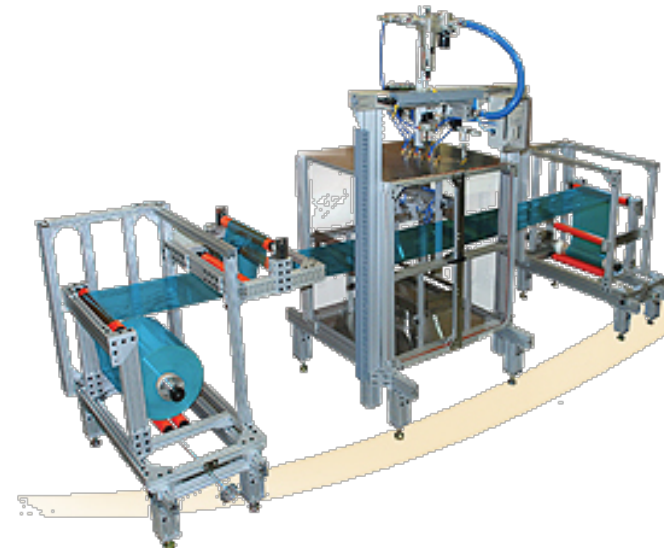
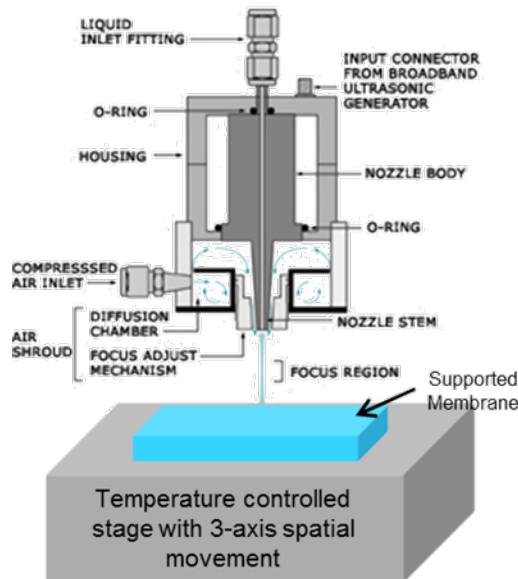


Bulk Material:	Gelled RTIL	Linear Poly(RTIL)/RTIL	Photo-curable Poly(RTIL)/RTIL	PVDF-co-HFP/RTIL
RTIL Loading (wt%):	98	40	80	80
CO ₂ Permeability (barrers):	950	105	650	650
CO ₂ /N ₂ Selectivity:	21	21	35	35
Physical Properties:	Mechanically weak	Brittle	Good	Good

Fabrication Approach 1: Ultrasonic Spray Coating

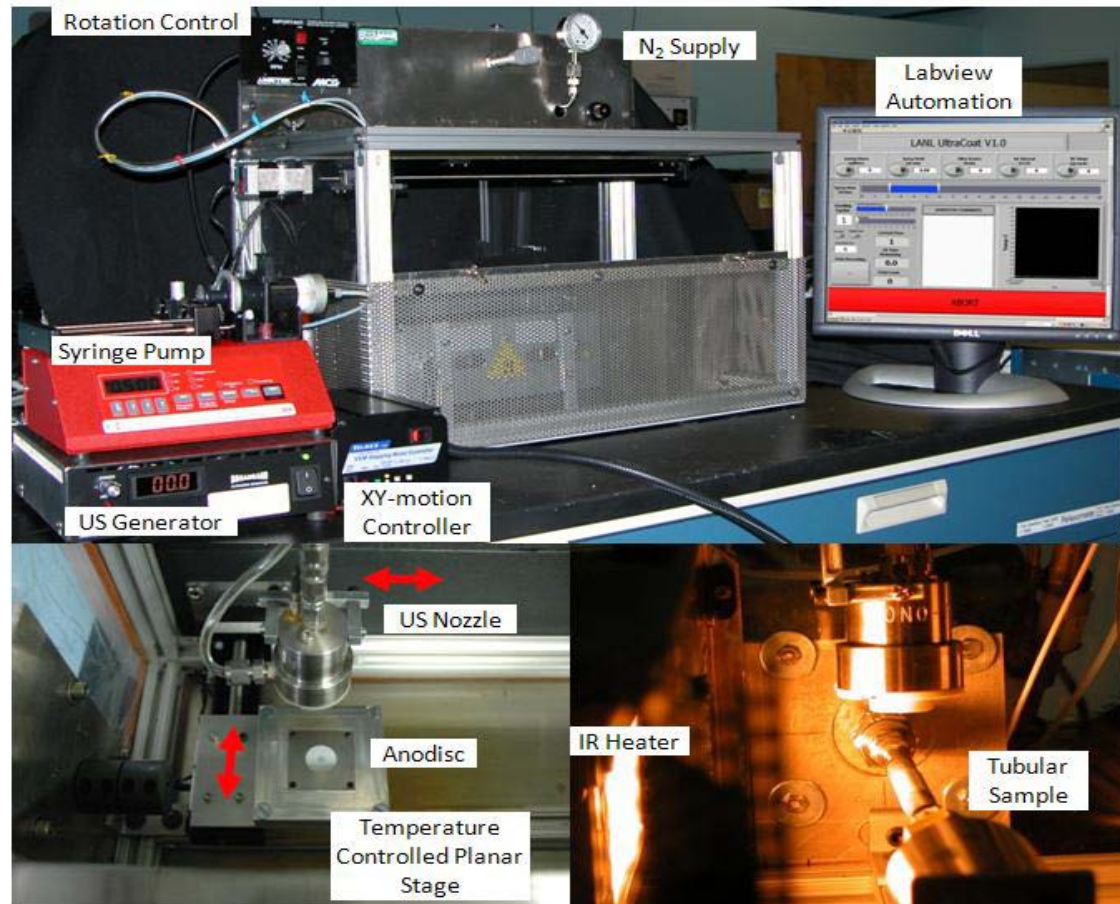
Ultra-Thin Membrane Fabrication, Optimization, & Testing

- Commercially viable fabrication technique development using ultrasonic spray-coating technology (USCT) -- enables controlled ultra-thin SL deposition on commercially attractive support platforms
- Maximize **Permeance** Attainable with **Selectivity Retention** -- defect mitigation with cohesive coating achieved



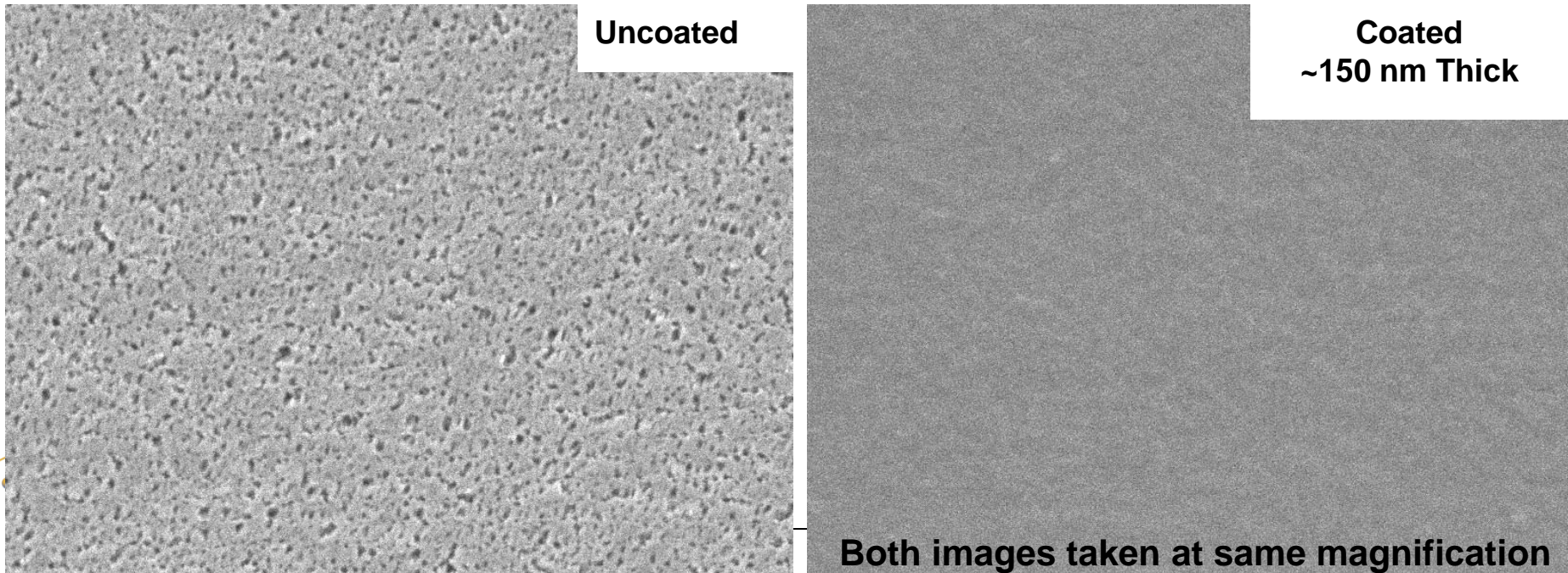
USCT-based Deposition

- Semi-automated small scale ultrasonic spray coating system for ultra-thin film deposition on tubular and planar substrates with *in-situ* processing
- System control parameters include:
 - Liquid flow rate
 - Spray geometry/profile
 - Coating profile / Raster speed
 - Substrate temperature
 - In-situ IR and UV irradiation
 - LabView® automation
 - Self-contained enclosure



RTIL based Ultra-thin Coating Development

- Developed methods to fabricate RTIL based selective layers on commercially attractive porous polymer supports
 - Numerous membranes fabricated to understand the effects of various coating parameters on selective layer deposition and its gas permeation characteristics
- Coating process optimization lead to 100-150 nm defect free coatings



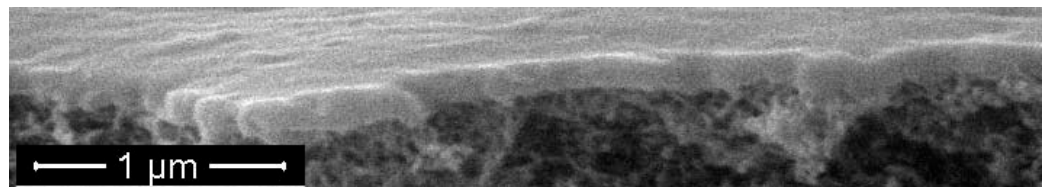
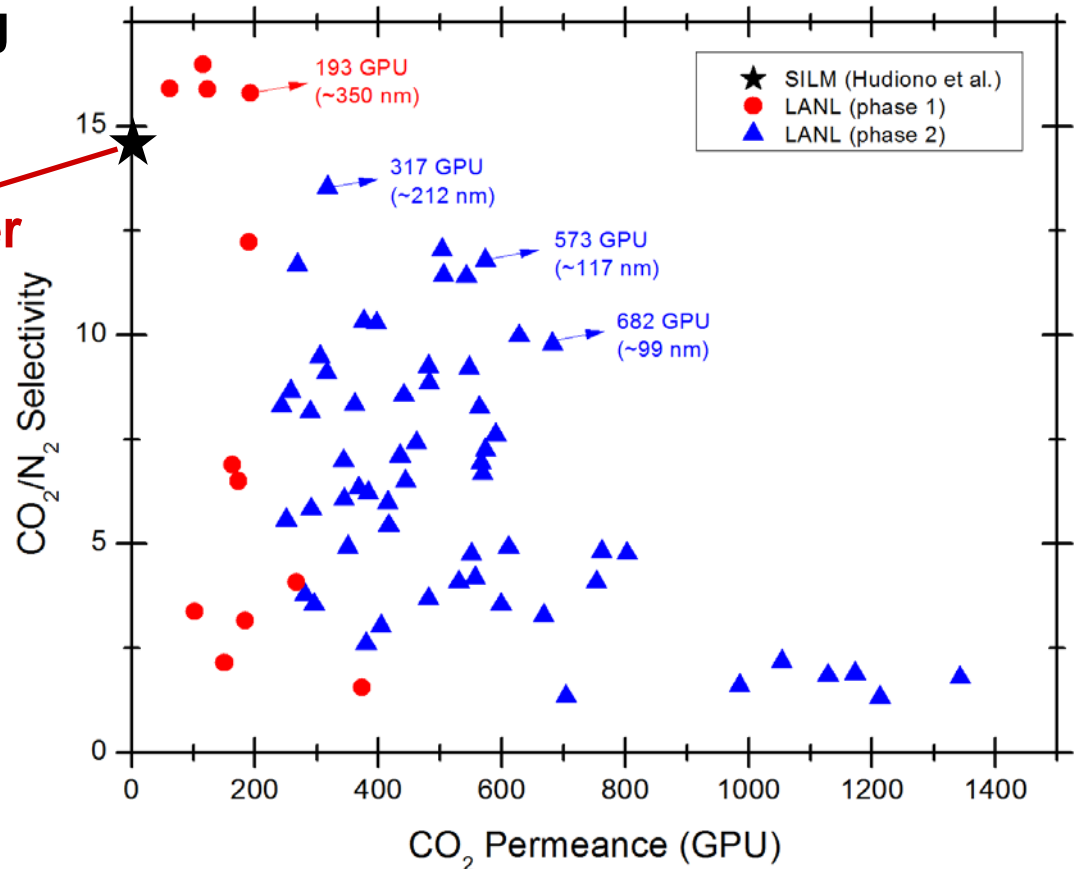
Ultra-thin Membrane Characterization

- Dramatic influence of coating parameters on membrane performance

Permeability = 67.3 barrer

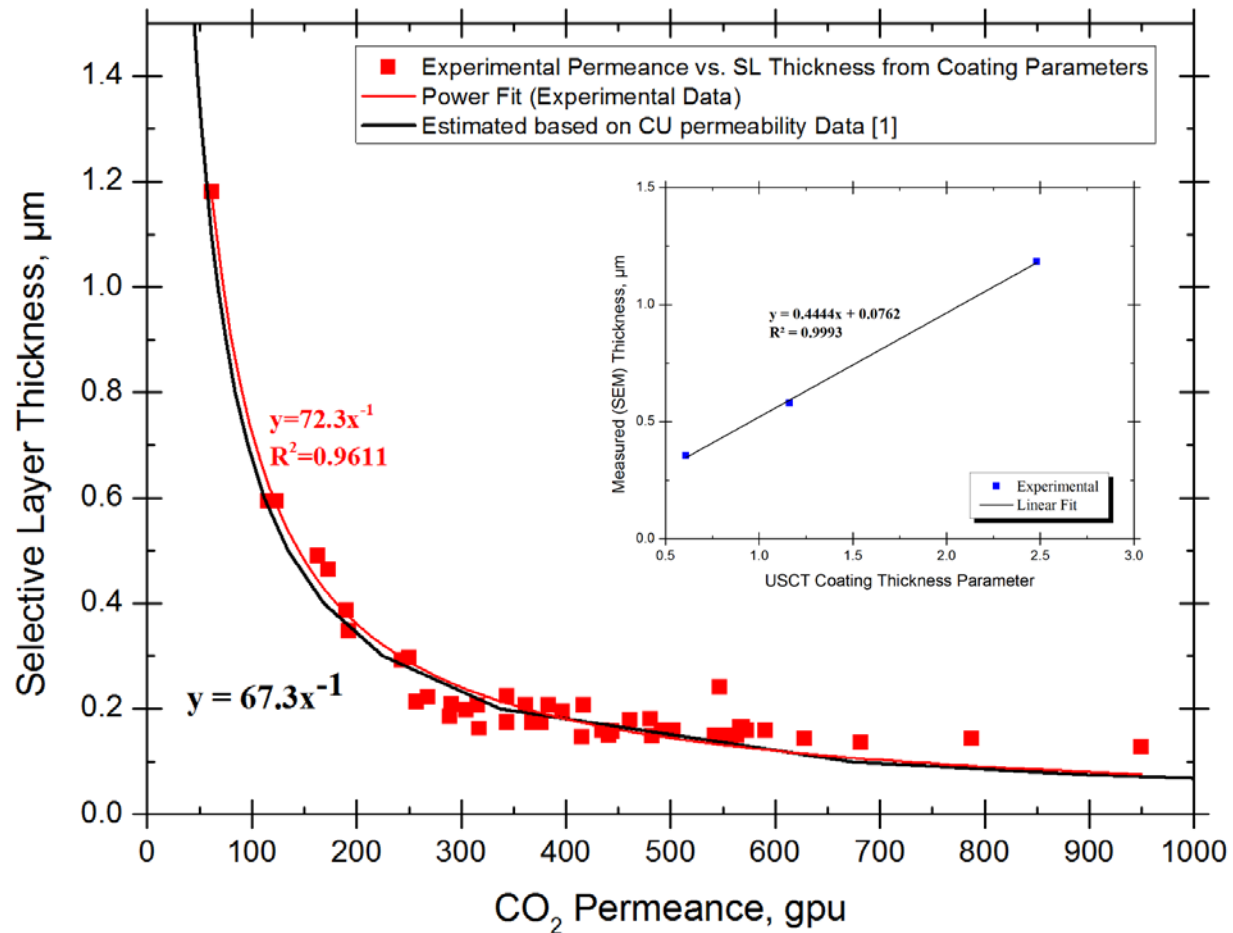
- Demonstrated defect-free poly(RTIL) composite membrane with CO₂ permeance of 317 GPU – approximately 212 nm effective thickness

- Fabricated numerous membranes with CO₂ permeance ≥ 500 and near ideal CO₂/N₂ selectivity ≥ 10



Controlling Membrane Fabrication Process

- Limited SEM thickness data set used for correlation with USCT coating thickness parameter (inset plot)
- Excellent correlation achieved between CO₂ permeance and estimated SL thickness
- Estimated permeability from composite membranes (72.3 barrer) in good agreement with CU permeability (67.3 barrer). (Membranes with CO₂/N₂ > 5 used in the analysis)

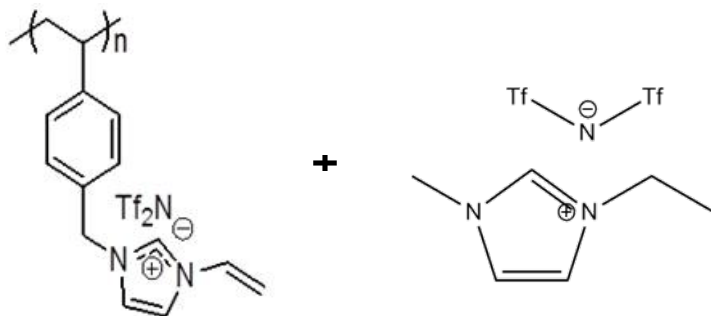


[1]: Hudiono Y.C. et al., *J. Membr. Sci.* **2011**, 370, 141-148

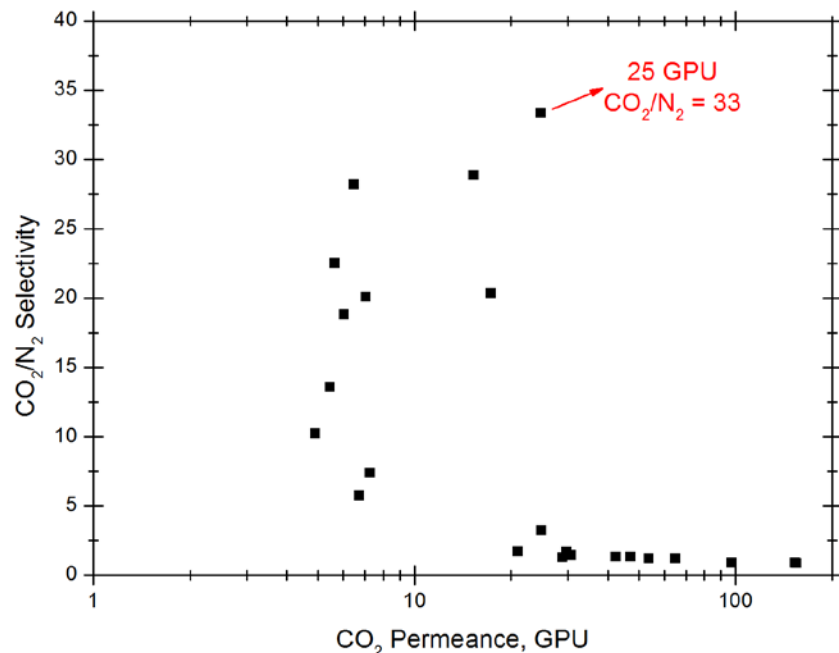
Fabrication of PSVI/RTIL Composite Membranes

Photocurable PSVI

RTIL: [emim][Tf₂N]



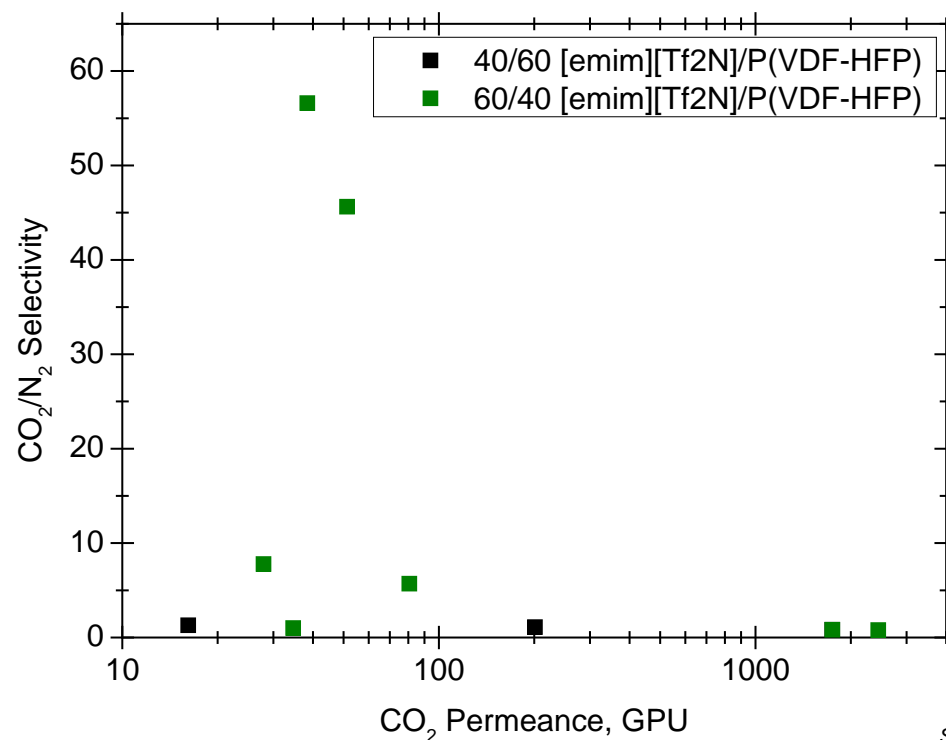
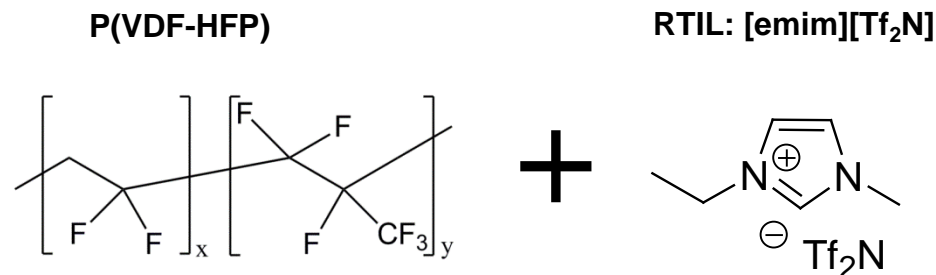
- High fraction of free RTIL (>50%) required to achieve high permeability
- Fabrication of PSVI-based composite membranes with varying RTIL ratios using USCT yields membranes with high CO₂/N₂ selectivity
- However, the permeances are much lower than expected from SILM data
 - With target thicknesses 1-2 μm, permeances are expected to be in the order of >100 GPU
 - Our best membrane fabricated using 80/20 PSVI/emim-Tf₂N, with CO₂/N₂ selectivity of 33, only has CO₂ permeance of 25 GPU (estimated selective layer thickness = 2 μm)



P(VDF-HFP)/emim-Tf₂N Composite Membranes

➤ Fabricated and evaluated p(VDF-HFP)/emim-Tf₂N composite membranes containing 40 and 60% emim-Tf₂N

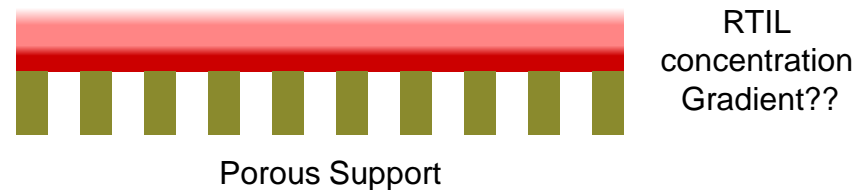
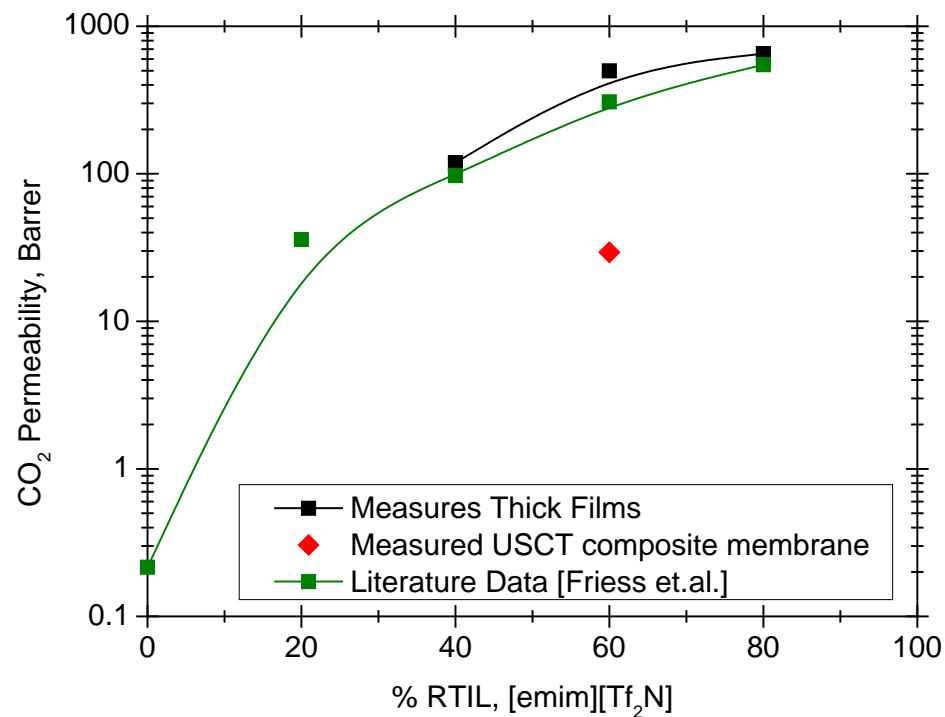
- Selective layer thickness varied from 0.2 to 1.8 μm
- High CO₂/N₂ selectivity obtained for 60/40 emim-Tf₂N/p(VDF-HFP) composite membrane with 0.9 μm thick selective layer!
- CO₂ permeance lower than that estimated from the CO₂ permeability obtained from bulk p(VDF-HFP)-RTIL composite films



Achieving High Permeance??

➤ Composite membranes fabricated by USCT have significant lower permeance than that estimated from the permeability data.

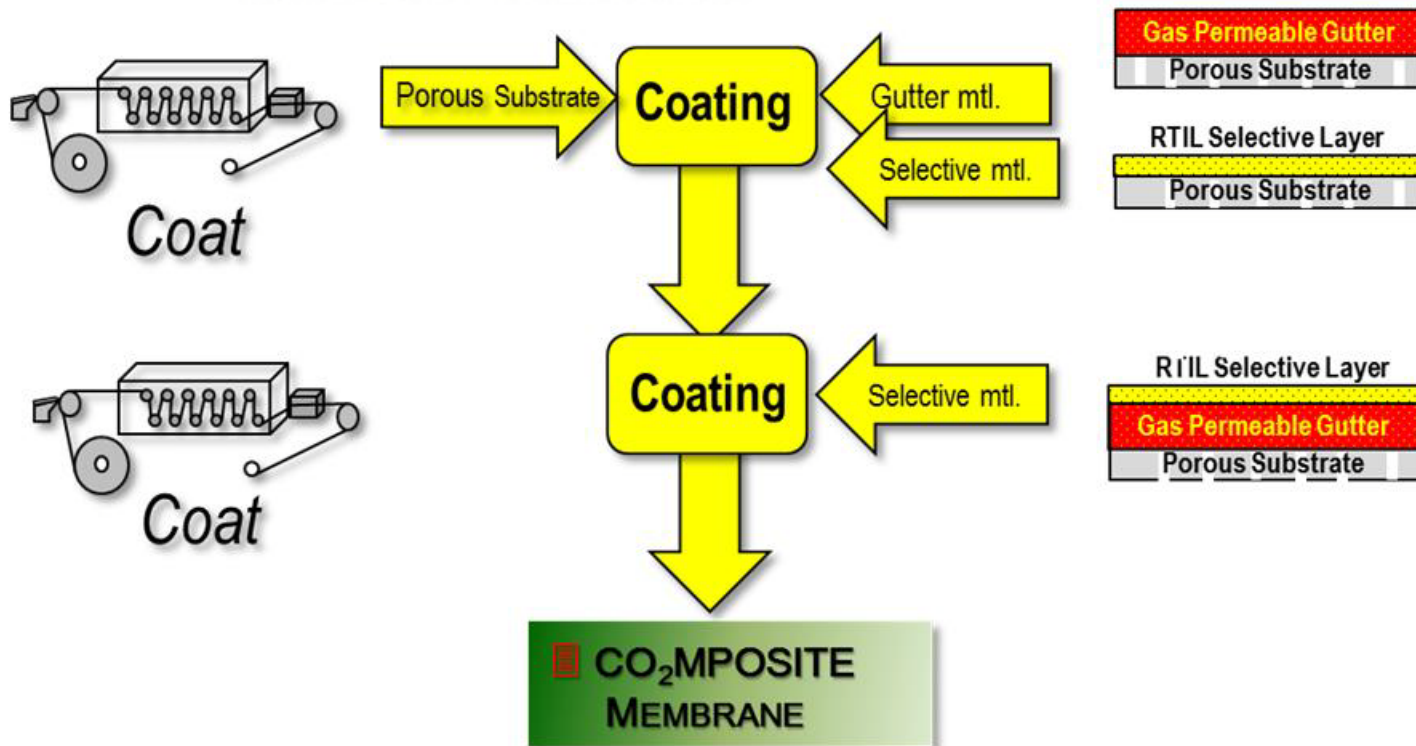
- Permeability of composite membrane with 60% free RTIL similar to permeability of film containing 20% RTIL
- Possible phase separation or RTIL migration to the support with solvent during coating leading to lower RTIL concentration in the selective layer.
- Pore penetration in the support pores increasing effective thickness.



Fabrication Approach 2: Roll to Roll Casting

- Direct single or multi-step coating on nano-porous substrate

DIRECT COATING

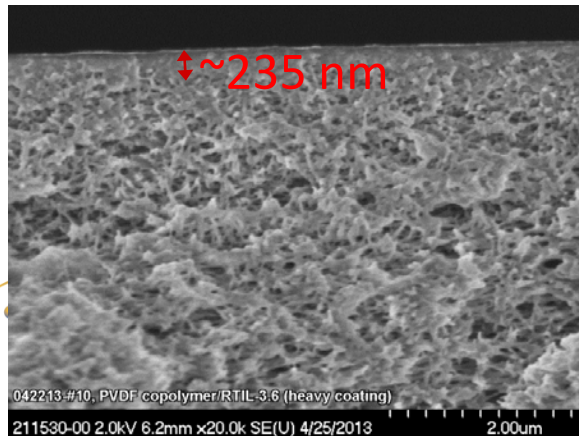


Direct Casting on Porous Substrate

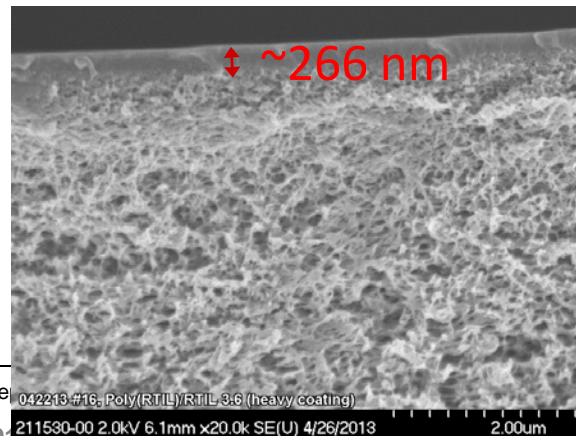
- **Selectivity observed - but low permeance**
 - **SEM cross sections show much thinner coatings than thickness targeted**
 - **Pore infiltration?**
 - **Free RTIL being carried into substrate by solvent?**

Sample	Target Thickness	Est. Obs. Thickness	CO ₂ Permeance	N ₂ Permeance	CO ₂ /N ₂ Selectivity
10-PVDF Comp.	2.8 um	235 nm	93	30	3.1
11B-PVDF Comp.	1.9 um	235 nm	73	30	2.4
16-PolyRTIL Comp.	2.8 um	266 nm	292	27	11
17-PolyRTIL Comp.	1.5 um	208 nm	292	28	10
20-PolyRTIL Comp.	1.5 um	117 nm	7730	917	8.4
24A-PolyRTIL Comp.	1.5 um	-	459	40	12

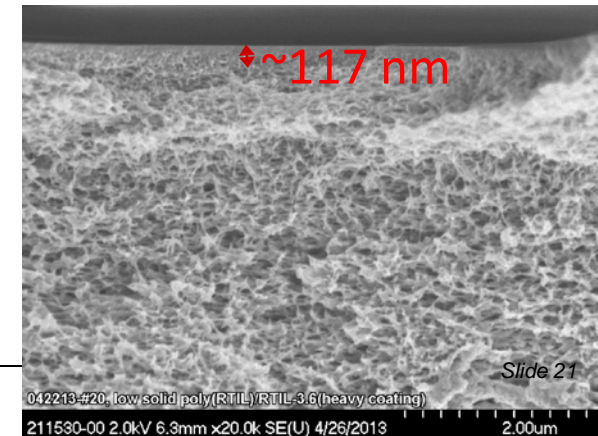
(10) PVDF Composite



(16) PolyRTIL Composite

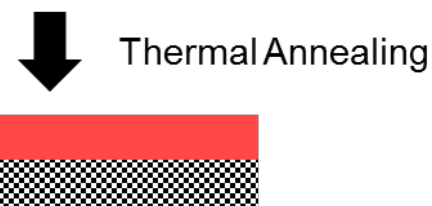
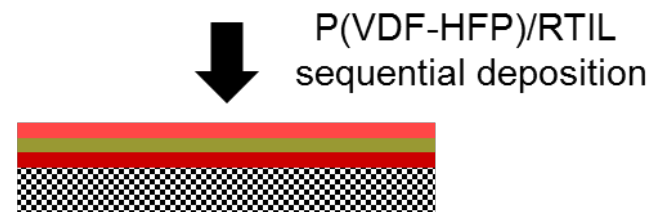
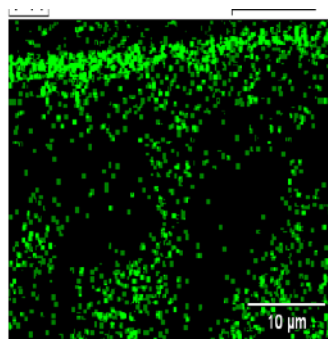
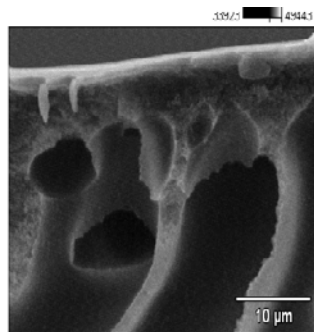


(20) PolyRTIL Composite



Newly Encountered Challenges for Thin Film Casting

- Discrepancy observed between measured bulk materials and thin film membrane properties
 - Hypothesis: Free RTIL being lost to porous substrate leaving majority polymer in coating
 - Elemental x-ray mapping confirms presence of fluorine in substrate

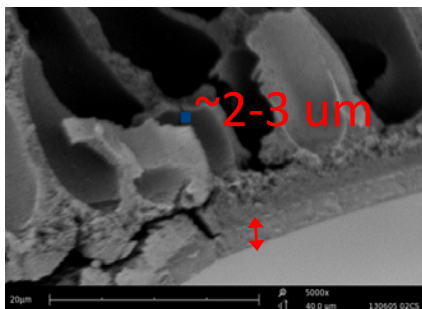


- Pure RTIL Layer
- P(VDF-HFP) layer with low RTIL loading
- P(VDF-HFP) layer with high RTIL loading

- Future Directions:
 - Optimize processing with RTIL rewetting procedure
 - Analytical characterization to understand RTIL-poly(RTIL) interactions

Preliminary Results: Secondary Coating & Post-Treatment

- Experiment:** Post-treat 2-3 um PVDF-HFP coating with pure free RTIL to promote diffusion
Result: Selectivity enhanced to bulk values; permeance appears unchanged



RTIL Post-Treatment	CO ₂ Permeance	N ₂ Permeance	CO ₂ /N ₂ Selectivity
None	16	16	1.0
50 C, 20 min	16	0.5	33
80 C, 5 min	22	0.7	30

- Experiment:** Apply secondary polymer/RTIL coating containing 75-80% free RTIL (Thickness ~200-300nm)
Result: Selectivity enhanced; permeance slightly reduced

Sample	Post-Treatment	CO ₂ Permeance	N ₂ Permeance	CO ₂ /N ₂ Selectivity
PVDF-HFP Comp. (240 nm)	None	93	30	3.1
	+ 2 nd Coating, 5 min at 50 C	32	5.6	5.7
	+ 2 nd Coating, 20 min at 50 C	64	6.5	9.8
PolyRTIL Comp. (270 nm)	None	290	27	11
	+ 2 nd Coating, 5 min at 50 C	230	12	18
	+ 2 nd Coating, 20 min at 50 C	240	14	17

Summary

- **Two classes of RTIL-based gel materials with bulk gas transport properties that meet the CO₂/N₂ permeability and selectivity targets were developed.**
- **Several examples of these two classes of RTIL-based gel materials were successfully cast at a thickness of 100 nm.**
- **A discrepancy between the bulk and composite membrane gas transport properties was observed.**
- **Several approaches to address this processing challenge have been developed and are being explored in earnest.**
- **Thorough analysis of the thin-film membranes produced to date is in progress.**
- **Preliminary modeling results technological and economic benefits over state-of-the-art CO₂ capture technology**
- **This work generated 7 published papers + 2 papers just accepted + 2 papers in preparation and 2 patent applications.**

Path Forward

➤ To Project Completion

- Develop a quantitative understanding of how the deposited material is distributed in the composite membrane both within the support and through the selective layer thickness.
- Multiple Layer coatings and post-processing to increase the permeability and selectivity of the final membrane.
- Complete parametric studies to further understand the influences of membrane performance characteristics on process economics.

➤ Transition to Commercialization

- In order to enhance the potential for industrial interest, we will also evaluate the membranes for CO₂/CH₄ separation (natural gas treatment) as requested by a petrochemical company. The selectivity target is CO₂/CH₄ selectivities >20 at low pressure and ambient temperature.

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